IN THE CLAIMS

Please amend the claims as follows:

- 1. (currently amended): A fixed-bed multitubular reactor, comprising:
- a plurality of reaction tubes to be packed with a catalyst;

catalyst temperature measures equipped to measure the temperature near the centre part in the radial direction of the reaction tubes;

a heat-medium bath located outside of said reaction tubes;

heat-medium bath temperature measures measuring temperatures of said heat-medium;

at least a portion of said plurality of reaction tubes being arranged so as to be adjacent to each other to form at least one reaction tube group; and

wherein the catalyst temperature measures being installed in all of the plurality of the reaction tubes or at least a part of said reaction tubes forming said at least one reaction tube group, the measurement positions thereof being different from each other in the longitudinal direction of the reaction tubes; and

the heat-medium bath temperature measures are equipped corresponding to the catalyst temperature measures so that the measurement positions Q thereof are set at the same height as the measurement positions P of the catalyst temperature measures.

2. (original) The fixed-bed multitubular reactor according to claim 1, wherein the catalyst temperature measurers are equipped in 5 to 35 tubes out of a reaction tube group comprising 5 to 105 reaction tubes adjacent to each other.

- 3. (previously presented): The fixed-bed multitubular reactor according to claim 2, wherein flow patterns of a heat medium are different in the reactor, and a plurality of the reaction tube groups are provided and respectively allocated to the positions where the flow patterns of the heat medium are different.

the catalyst temperature measures being installed in all of the plurality of the reaction tubes or at least a part of said reaction tubes forming the reaction tube group, the measurement positions thereof being different from each other in the longitudinal direction of the reaction tubes oxidizing a gas in the fixed-bed multitubular reactor of claim 1.

- 5. (currently amended) The fixed bed multitubular reactor method according to claim 4, wherein the gas-phase catalytic oxidation reaction is a reaction synthesizing an unsaturated aldehyde or an unsaturated carboxylic acid from propylene, isobutylene or tertiary butyl alcohol.
- 6. (currently amended) The fixed-bed multitubular reactor method according to claim 4, wherein the gas-phase catalytic oxidation reaction is a reaction synthesizing an unsaturated carboxylic acid from an unsaturated aldehyde.

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7. (cancelled)

8. (previously presented): The fixed-bed multitubular reactor according to claim 1,

wherein a plurality of the reaction tubes groups are allocated circularly and at least one

reaction tube group is allocated in each section L which is made by separating the cross

section of the reactor in the radial direction from the centre M into two or more sections

having the same area.

9. (previously presented): The fixed-bed multitubular reactor according to claim 1,

wherein the length of the reaction tube is 2 to 7 meters.

10. (previously presented): The fixed-bed multitubular reactor according to claim 1,

wherein the setting interval of the catalyst temperature measures is from 0.1 to 2 meters.

11. (previously presented) The fixed-bed multitubular reactor according to claim 1,

comprising a plurality of reaction tube groups arranged in a triangular configuration.

12. (previously presented) The fixed-bed multitubular reactor according to claim 1,

comprising a plurality of reaction tube groups arranged in a square configuration.

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